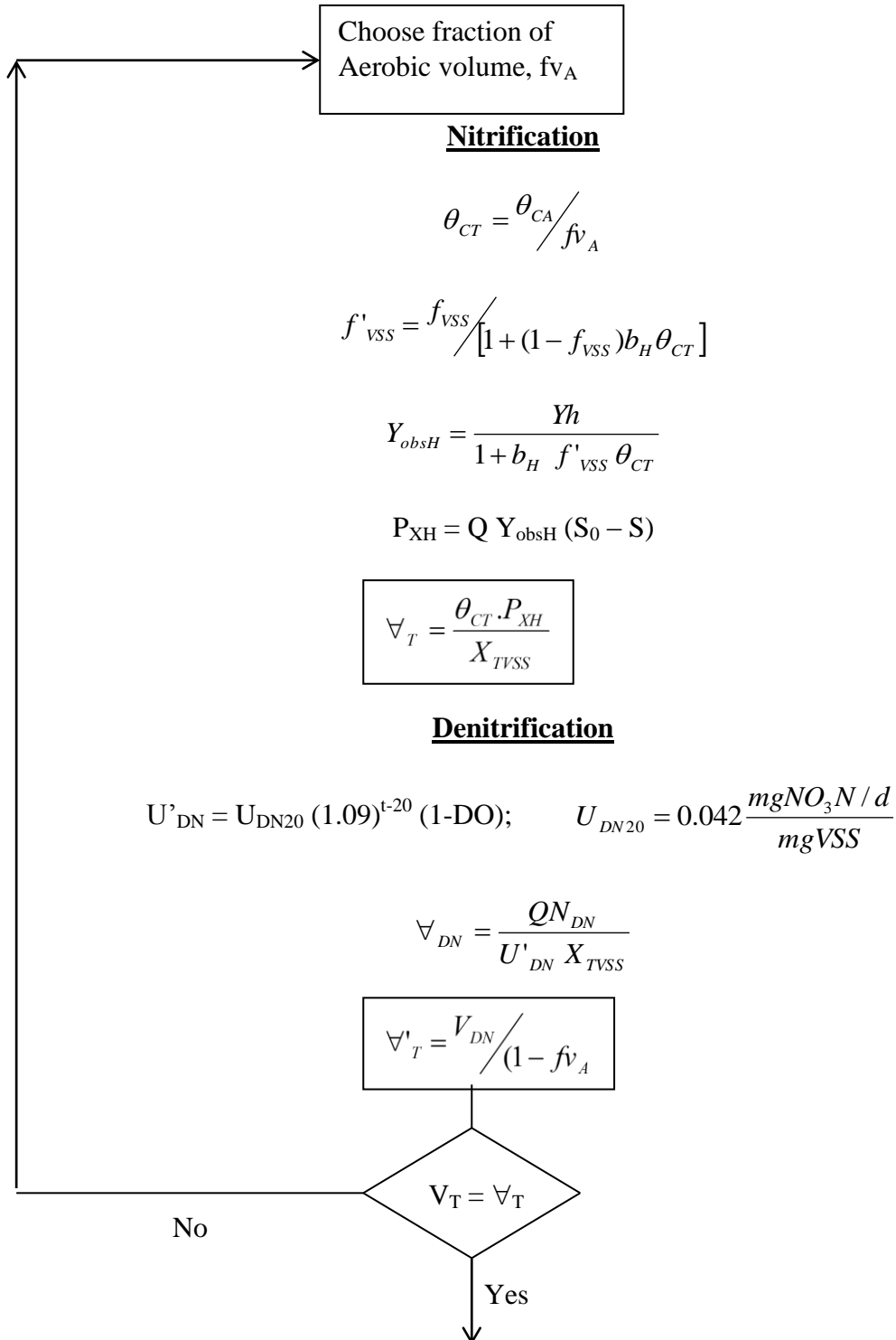


LAWRANCE & McCARTHY METHOD

Calculate θ_{CA}

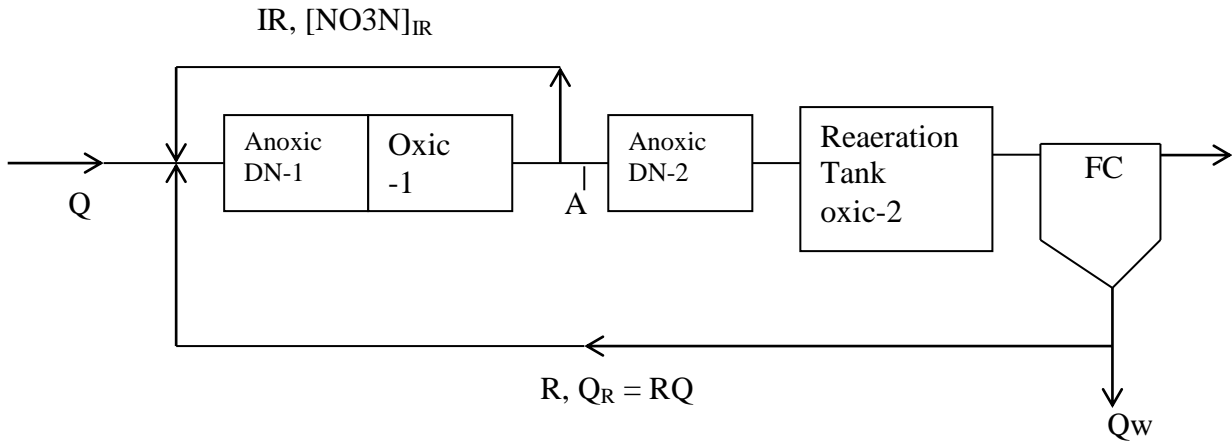
$$\mu'_{\max A} = \mu e^{0.098(t-15)} \frac{DO}{K_{DO} + DO} [1 - 0.833(7.2 - pH)]$$

$$\theta_{CA} = \frac{(SF_{kinetic})(SF_{process})}{\mu'_{\max A} - b_A}$$



WEF MOD BARDENPHO DESIGN

5 Stage Bardenpho Process



Calculation of the Oxic Volume V_A

Single Sludge, Seperate Stage

$$\mu'_A = \mu e^{0.098(T-15)} \frac{DO}{K_{DO} + DO}$$

$$\text{Design } \theta_{CA} = \theta_{CA} = \frac{1}{\mu'_A - b_A}$$

System $\theta_{CT} = (1.8 - 2.0) \theta_{CA}$

$$Y_{obsH} = \frac{Y_H}{(1 + b_H f_{VSS} \theta_{CT})}$$

$$\theta_{CT} = \frac{V_T X_{TVSS}}{Q Y_{obsH} (S_0 - S)}$$

$$\theta_{CA} = \frac{V_A X_{TVSS}}{Q Y_{obsH} (S_0 - S)} \quad \rightarrow \quad V_A = \frac{Q \theta_{CA} Y_{obsH} (S_0 - S)}{X_{TVSS}}$$

V_{DN-1} First Anoxic Zone Pre-Denitrification (Exogenous Pre-Denitrification)

$$[NO_3N]_{IR} = \frac{TKN \text{ to Nitrif}}{Q + Q_R + Q_{IR}}$$

$[NO_3N]_{IR}$ is also the concentration at the inlet of V_{DN-2} (pt A)

$$\text{NO}_3\text{N to be DN} = Q (\text{IR}) [\text{NO}_3\text{N}]_{\text{IR}} + Q_{\text{R}}[\text{NO}_3\text{N}]_{\text{eff}}$$

$$r_{\text{DN-1}} = \frac{\text{NO}_3\text{N to be DN in the 1}^{\text{st}} \text{ anoxic zone}}{\forall_{\text{DN-1}} X_{\text{TVSS}}}$$

Solve for $\forall_{\text{DN-1}}$ assuming that the DN Rate in the first anoxic pre-DN zone of Bardenpho is given by the eqn:

$$r_{\text{DN-1}} = \left[0.03 \frac{F}{M} + 0.029 \right] (1.06)^{t_c - 20}$$

$$\frac{F}{M} = \frac{Q(S_0 - S)}{\forall_{\text{DN-1}} X}$$

Post Denitrification

2nd Anoxic Zone, observed in 2nd anoxic tank of the Bardenpho Process (Endogenous Denitrification)

$$r_{\text{DN-2}} = 0.12 \theta_{\text{CT}}^{-0.706} (1.03)^{t_c - 20}$$

NO_3 to be DN in $\forall_{\text{DN-2}} = \text{TKN}_{\text{oxidized}} - \text{NO}_3\text{N removed in } \forall_{\text{DN-1}} - \text{NO}_3\text{N}_{\text{eff}}$

$$X \forall_{\text{DN-2}} = \frac{\text{NO}_3 \text{ to be DN in } \forall_{\text{DN-2}}}{r_{\text{DN-2}}}$$

Additional second anoxic zone tank volume required to take up the DO in the aeration tank effluent.

$$\text{Specific OUR} = \frac{A_n}{Y_h \theta_{\text{CT}}} * \text{MLSS} [=] \text{mgO}_2 / \text{h} / \text{L}$$

Add $\forall_{\text{DN-2}} = 0.5 \text{ mg/L/S}_{\text{POUR}} * Q_{\text{design}}/24$

$$\forall_{\text{DN-2}} = \forall'_{\text{DN-2}} + \forall_{\text{DN-2 Additional}}$$

Reaeration Tank

Calculate the volume for 45 min retention time at average day/maximum month flow.

COMPARISON OF BNR DESIGN METHODS

THE WEF METHOD

The WEF method is essentially the same as the Lawrence & McCarthy Method only the trial and error solution is not made and θ_{CT} is assumed to be approximately twice of θ_{CA} . In the WEF method two different equations for exogenous and endogenous denitrification rates are used. The nitrate amount to be denitrified includes the internal recirculation ratio. The aerobic volume and the total volumes are calculated using θ_{CA} and θ_{CT} respectively.

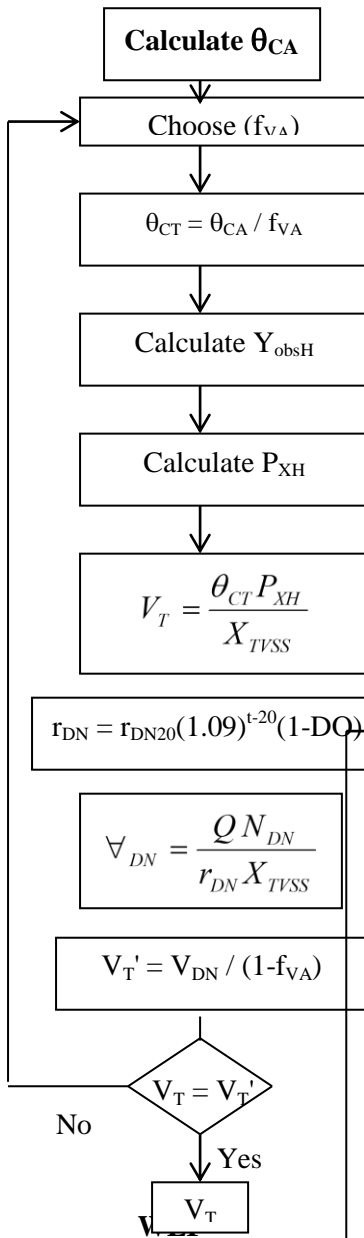
COMPARISON OF QASIM & LAWRENCE & MCCARTY METHODS

While Qasim calculates Y_{obs} for denitrification (Y_{obsDN}) and for BOD removal ($Y_{obsBOD5}$) as separate constants using aerobic θ_C , Lawrence & Mc Carthy Method calculates one Y_{obs} for heterotrophic Bacteria using total θ_C (θ_{CT}).

Lawrence & Mc Carthy Method, Qasim's method uses a mean cell residence time equation (θ_{CDN}) for denitrification volume (V_{DN}), calculations and a trial and error solution is used till total volume V_T calculated using V_{DN} and fraction of aerobic volume equals to the V_T calculated using total mean cell residence time θ_{CT} also calculated from θ_{CA} using the assumed fraction of aerobic volume.

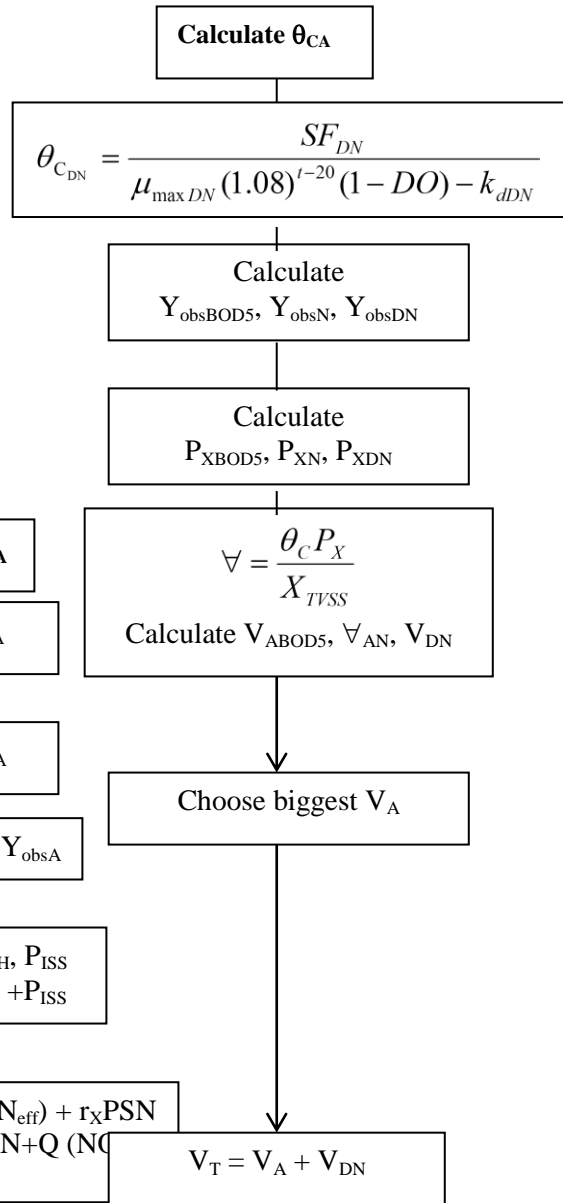
Every program should share a carbon and nitrogen balance, oxygen requirements subroutines in addition to oxic and anoxic volumes.

Lawrance & Mc Carthy

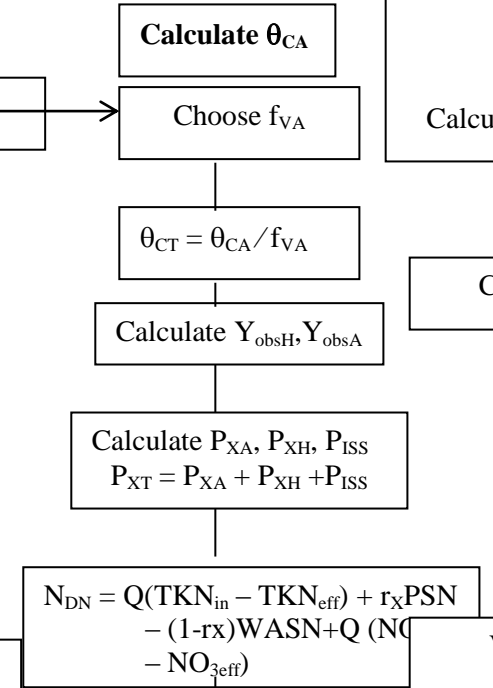


$$V_T = \frac{\theta_{CT} P_{XT}}{X_{TVSS}}$$

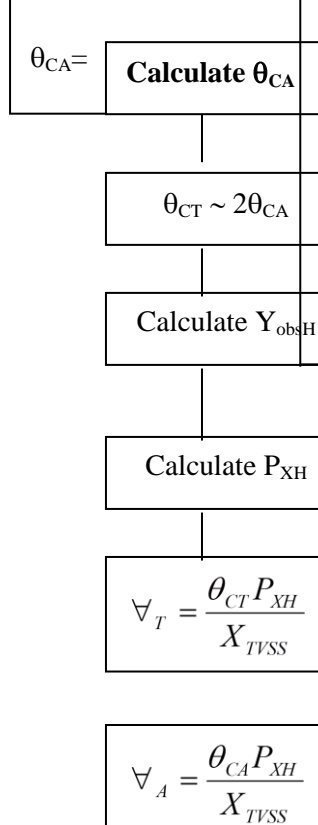
Qasim



ATV131



Modified Lawrance



$$V_A = V_T f_{VA}$$

$$V_{DN} = V_T - V_A$$

θ_{CA} CALCULATION

$$\mu'_{\max A} = \mu e^{0.098(t-15)} \frac{DO}{DO + K_{DO}} [1 - 0.833(7.2 - pH)]$$

$$\theta_{CA} = \frac{(SF_{kinetic})(SF_{process})}{\mu'_{\max A} - k_{dA}}$$

Y_{obs} & P_X CALCULATIONS

VOLUME CALCULATIONS

$\theta_{CDN} = \frac{SF_{DN}}{\mu_{\max DN} (1.08)^{t-20} (1 - DO) - k_{dDN}}$ $P_{XDN} = Y_{obsDN} Q(N_{DN})$	$\nabla_{DN} = \frac{(\theta_{CDN}) P_{XDN}}{f_{XDN} X_{TVSS}}$ $f_{XDN} = 0.5$	<p style="text-align: center;"><u>NITROGEN</u></p> $N_{DN} = N_{N-} - (NO_3N_{eff})$ $N_N = TKN_{in} - TKN_{eff} - C$ OrgNassim = 0.122 Y
$Y_{obsBOD_5} = \frac{Y_{BOD_5}}{1 + k_{dBOD_5} (\theta_{CA})}$ $P_{XBOD_5} = Y_{obsBOD_5} Q(\text{BOD}_5 \text{ to satisfy})$	$\nabla_{ABOD_5} = \frac{(\theta_{CA}) P_{XBOD_5}}{f_{XH} X_{TVSS}}$ $f_{XH} = 0.94$	<p style="text-align: center;"><u>CARBON</u></p> $BOD_5 \text{ to satisfy} = (S_0 - S) X \left(\text{for } \dots \right)$
$Y_{obsN} = \frac{Y_N}{1 + k_{dN} (\theta_{CA})}$ $P_{xN} = Y_{obsN} Q(N_N)$	$\nabla_{AN} = \frac{(\theta_{CA}) P_{xN}}{(f_{xA})(X_{TVSS})}$ $f_A = 0.06$	$(BOD_5 \text{ for DN}) = 0.68$ $(BOD_5 \text{ for Deoxygen}) = 0.68 (1.3) [0.122 Y]$
$Y_{obsDN} = Y_{DN} / (1 + k_{dDN} \theta_{CDN})$ $Y_{obsBOD_5} = Y_{BOD_5} / (1 + k_{dBOD_5} \theta_{CA})$	Choose biggest ∇_A $\nabla_T = \nabla_{DN} + \nabla_A$	

QASIM EX 13 - 11 IN A NUT SHELL

7 Methods of BNR Design

1. Trial & Error (Lawrance & Mc Carthy)
Model I, Model II
2. DN Capacity (ATV-131)
3. DN rate eqn (WEF)
4. Cowi Design
5. Kruger Design

6. IA WPRC Task Group

7. Qasim Ex 13 - 11

