

## SLUDGE PRODUCTION FROM BIO-P REMO

Q=	42500	m <sup>3</sup> /d
BOD <sub>0</sub> =	300	mg/L
P <sub>in</sub> =C <sub>p,IAT</sub>	10	
P <sub>eff</sub> =C <sub>p,ES</sub>	1	

### PxT

Y <sub>obsH</sub> =	0.697	Y <sub>obsH</sub> = (0,75+0,6(SS/BOD))-((1-0,2)*0,17*0,75)
SP <sub>d,C</sub> =	8,887 kg/d	=Y <sub>obs</sub> *Q*BOD <sub>0</sub> /1000
X <sub>p,BM</sub> =	3.00 mg/L	=Q*0.010*BOD <sub>0</sub> /1000 Biological P
X <sub>p,bioP</sub> =	3.00 mg/L	=Q*0.010*BOD <sub>0</sub> /1000
X <sub>p,prec</sub> =	3.00 mg/L	=(T <sub>Po</sub> -T <sub>Peff</sub> -X <sub>p,BM</sub> -X <sub>p,BioP</sub> )/(T <sub>Po</sub> -T <sub>Peff</sub> -0.01)
SP <sub>d,P</sub> =	1,249.50 kg/d	=Q*(3*X <sub>p,bioP</sub> +6.8*X <sub>p,prec</sub> )/1000
P <sub>xT</sub> =	10,136.25 kg/d	=SP <sub>d,C</sub> +SP <sub>d,P</sub>

Reference: ATV-131-A

$$X_{P, Prec} = C_{P, IAT} - C_{P, EST} - X_{P, BM} - X_{P, BioP}$$

$C_{P, IAT}$  is the concentration of the total phosphorus in the influent.  $C_{P, EST}$  is to be set as the effluent concentration of phosphorus ( $C_{P, ER}$ ), e.g.  $C_{P, EST} = 0.6$  to  $1.0$  mg/L.  $X_{P, BM}$  can be set as the concentration of heterotrophic biomass in the aeration tank.  $X_{P, BioP}$  can be set as the concentration of phosphorus in the anaerobic tanks. For normal municipal wastewater one can assume a phosphorus removal of 90%.

—  $X_{P, BioP} = 0.01$  to  $0.015 \cdot C_{BOD, IAT}$  or  $0.005$  to  $0.01$  mg/L in anaerobic tanks.

of precipitant and the amount of dosing, the production of 2.5 kg SS per kg dosed iron and the production resulting from phosphorus removal.

$$SP_{d, P} = Q_d \cdot (3 \cdot X_{P, BioP} + 6.8 \cdot X_{P, Prec})$$

If lime is used for precipitation the sludge  
( $\text{Ca}(\text{OH})_2$ ); see also ATV Standard ATV-A 2

# VAL AND P PRECIPITATION WITH FeCl3

$(1+0,17 \cdot \text{SRT} \cdot \text{FT})$

Organic Matter resulting from de

removed (0,01-0,015 of BOD Load)

SOLID MATTER FROM EXCESS BIO-P REMO

SOLID MATTER FROM simultaneous pp

$\cdot \text{BOD}_0 - 0,01 \cdot \text{BOD}_0$ )

Concentration of P to be precipitated

TOTAL SLUDGE

$$X_{P, \text{BioP}} \quad [\text{mg/l}] \quad (5-9)$$

osphorus in the influent to the biological reactor. The  
 elected in agreement with the effluent requirement for  
 $0,7 C_{P, \text{ER}}$ . The phosphorus necessary for the build-up  
 t as  $0,01 C_{\text{BOD, IAT}}$  or  $0,005 C_{\text{COD, IAT}}$  respectively. With  
 ume the following for the excess biological phosphorus

05 to  $0,007 C_{\text{COD, IAT}}$  respectively with upstream

comp. Sect. 5.2.3. One should reckon with a sludge  
 and 4 kg SS per kg dosed aluminium. The total sludge  
 val ( $\text{SP}_{d, P}$ ) thus results as follows:

$$c_{, \text{Fe}} + 5,3 \cdot X_{P, \text{Prec, Al}} / 1000 \quad [\text{kg/d}] \quad (5-14)$$

production is 1.35 kg SS per kg calcium hydroxide  
202.

gradation and stored solid matter

DVAL (Bio-P Tanks)  
tn (FeCl<sub>3</sub> addm)

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